

Minor Source nination Number er: 25127 escription: ing/Capacity: ocation:	ə r : 141	BACT Determination Date: Information Expires - 9/3	OFFEE ROASTI 9/4/2019 8/9021
er: 25127 escription: ing/Capacity:	Equipment COFFEE ROASTER < 110,000 Btu/hr VINTAGE PRODUCTIO 2827 S ST	Information Expires - 9/3	
escription: ing/Capacity:	COFFEE ROASTER < 110,000 Btu/hr VINTAGE PRODUCTIC 2827 S ST	Expires - 9/3	2/9091
escription: ing/Capacity:	< 110,000 Btu/hr VINTAGE PRODUCTIC 2827 S ST	-	3/9091
ing/Capacity:	< 110,000 Btu/hr VINTAGE PRODUCTIC 2827 S ST	-	2/2021
• • •	VINTAGE PRODUCTIO 2827 S ST	-	
ocation:	2827 S ST	ON CALIFORNIA LLC	
	-		
	SACRAMENTO, CA		
	BACT Determina	tion Information	
tandard:	≥ 90% control efficiency		
echnology	Afterburner (0.3 second retention	on time at 1200 °F) or equivalent technology	
escription:			
asis:	Achieved in Practice		
tandard:			
echnology	Natural gas fuel		
escription:			
asis:	Achieved in Practice		
tandard:			
echnology	Natural gas fuel		
escription:			
	Achieved in Practice		
	Natural gas fuel with cyclone ar technology	nd afterburner (0.3 second retention time at 1200 °	F) or equivalent
	Achieved in Practice		
	Cyclone and natural gas fuel		
	-, -, -, -, -, -, -, -, -, -, -, -, -, -		
•	Achieved in Practice		
tandard:			
echnology	Natural gas fuel and good com	oustion practices	
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Expires - 9/3/2021

CATEGOR	Y:	CO	FFEE ROASTER	
BACT Size:	Minor Source	BACT		COFFEE ROASTE
BACT Dete	ermination Numb	er: 184	BACT Determination Date:	9/4/2019
		Equipmer	nt Information	
Unit Size/F	mber: N/A t Description: Rating/Capacity: t Location:	Generic BACT Determina COFFEE ROASTER 110,000 Btu/hr to 3.5		3/ 2021
		BACT Determin	nation Information	
ROCs	Standard:	≥ 90% control efficiency		
RUUS	Technology Description:	afterburner (0.3 second reten	tion time at ≥1400 °F) or equivalent technology	
	Basis:	Achieved in Practice		
NOx	Standard: Technology	40 or 60 ppm NOx at 3% O2, For units ≥ 325,000 BTU/hr: I	see comments Low NOx burner, see comments for details	
	Description: Basis:	Achieved in Practice		
Technology Natural gas fuel Description:				
	Basis: Standard:	Achieved in Practice		
PM10	Technology Description:	Natural gas with cyclone and technology	afterburner (0.3 second retention time at 1400 $^\circ \mathrm{F})$	or equivalent
	Basis:	Achieved in Practice		
PM2.5				
	Basis:	Achieved in Practice		
CO	Standard: Technology Description: Natural gas fuel and good combustion practices			
	Basis:	Achieved in Practice		
LEAD	Standard:			
	Technology Description: Basis:			
Comments	 BACT for NOx: 1.40 ppm NOx at 3⁴ roaster burners ≥ 5⁶ 	00 °F % O2 or 0.073 lb/MMBtu for afte	aster burners < 500 °F, 60 ppm NOx at 3% O2 or 0.0 erburners, thermal oxidizers, catalytic oxidizers, and b) 874-4863 email: jquok@airquality	l vapor incinerators

777 12th Street, Third Floor

SACRAMENTO METROPOLITAN

Sacramento, CA 95814





BEST AVAILABLE CONTROL TECHNOLOGY DETERMINATION

	DETERMINATION NO .:	141 & 184
	DATE:	September 4, 2019
	ENGINEER:	Jeffrey Quok
Category/General Equip Description:	Coffee Roaster	
	Coffee Roaster < 110,00	0 Btu/hr (BACT #141)
Equipment Specific Description:	Coffee Roaster 110,000 (BACT # 184)	Btu/hr to 3.5 MMbtu/hr
Equipment Size/Rating:	Minor Source BACT	
Previous BACT Det. No.:	100	

This BACT/T-BACT determination will update Determination #100 for Coffee Roasters.

This BACT/T-BACT was determined under the project for A/C 25127 (Temple Coffee).

BACT ANALYSIS

A: ACHIEVED IN PRACTICE (Rule 202, §205.1a):

The following control technologies are currently employed as BACT for coffee roasters by the following air pollution control districts and agencies:

District/Agency	Best Available Control Technology (BACT)/Requirements			
BACT Source: EPA RACT/BACT/LAER Clearinghouse				
	Coffee	Roaster		
	VOC	N/A – No BACT determinations found		
	NOx	N/A – No BACT determinations found		
US EPA	SOx	N/A – No BACT determinations found		
	PM10	N/A – No BACT determinations found		
	PM2.5	N/A – No BACT determinations found		
	CO	N/A – No BACT determinations found		
		·		

District/Agency	Best Available Control Technology (BACT)/Requirements			
US EPA	<u>T-BACT</u> There are no T-BACT standards published in the clearinghouse for this category. <u>RULE REQUIREMENTS</u> : None			
	BACT Source: ARB BACT Clearinghouse			
	Coffee	Roaster		
	VOC	N/A – No BACT determinations found		
	NOx	N/A – No BACT determinations found		
	SOx	N/A – No BACT determinations found		
	PM10	N/A – No BACT determinations found		
ARB	PM2.5	N/A – No BACT determinations found		
	СО	N/A – No BACT determinations found		
	RULE REQUIREMENTS: None BACT			
	Source: SMAQMD BACT Clearinghouse (1/30/15)			
	Coffee F			
	VOC	≥ 90% control efficiency		
	NOx	Natural Gas Fuel		
	SOx	Natural Gas Fuel		
	PM10	Cyclone and Natural Gas Fuel		
SMAQMD	PM2.5 CO	Cyclone and Natural Gas Fuel Natural gas fuel and good combustion practices		
	T-BACT There ar category. RULE RE Rule 419 This Rule total rated major sta cooking u	e no T-BACT standards published in the clearinghouse for this		

District/Agency	Best Available Control Technology (BACT)/Requirements						
	The requirements of this rule do not apply to combustion equipment where its primary function is to operate as an air pollution control device including, but not limited to, afterburners, catalytic oxidizers, flares, thermal oxidizers, or vapor incinerators.						
SMAQMD		TA Emission Limits Exp	BLE 2: Cooki pressed As Pl		cted to 3% O ₂		
	Equipment Category		NOx L ppmv, cor 3% (Ib/MM	imit rected to O ₂	CO Limit ppmv, corrected to 3% O ₂ (Ib/MMBtu)		
			Eff	ective (see	Section 401)		
	Gas	eous Fuel-Fired Equipment	Proc Tempe	rature	All Temperatures		
	Cooking		< 500°F 40 (0.049)	≥ 500 °F 60 (0.073)	800 (0.60)		
	BACT Source: <u>SCAQMD BACT Guidelines for Non-Major Polluting Facilities, page</u> <u>33</u> (2/1/2019)						
	Coffee I	Roaster, < 110,000 B	TU/hr				
	VOC	No standard					
	NOx	Compliance with Ru	ule 1147				
	SOx	Natural Gas					
	PM10	Natural Gas					
	PM2.5	No standard					
South Coast	со	No standard					
AQMD	Coffee F	Coffee Roaster, ≥ 110,000 BTU/hr					
	VOC	Afterburner (0.3 second retention time at 1200 °F)					
	NOx	Compliance with Ru	ule 1147				
	SOx	Natural Gas					
	PM10	Natural Gas with cyclone and afterburner (0.3 second retention time at 1200 °F)					
	PM2.5	No standard					
	СО	No standard					
	T-BACT	e no T-BACT stan	dards publisl	ned in the	clearinghouse for this		

District/Agency	Best Available Control Technology (BACT)/Requirements					
	RULE REQUIREMENTS:					
	Reg XI, Rule 1147 – NOx Reductions from Miscellaneous Sources (7/7/2017) The purpose of this rule is to reduce nitrogen oxide emissions from gaseous and liquid fuel fired combustion equipment as defined in the rule.					
	The rule requires than on or after January 1, 2010 any person owning or operating a unit subject to the rule shall not operate the unit in a manner that exceeds the applicable nitrogen oxide emission limits specified in Table 1 at the time a District permit is required for operation of a new, relocated or modified unit. The NOx emission limits of Table 1 only apply to units greater than or equal to 325,000 BTU/hr.					
South Coast AQMD	Per section (g)(2), the provisions of this rule shall not apply to charbroilers or food ovens. Food oven means an oven, cooker, dryer, roaster, or other fuel- fired unit, excluding fryer, used to heat, cook, dry, roast, or prepare food, food products, or products used for making beverages for human consumption. Since a coffee roaster is used to roast products used for making beverages for human consumption, coffee roasters are exempt from this rule. However, afterburners are still applicable.					
			x Emission Limit fo	-		
	Equipment Categories	Ratings ≥ 325,000 BTU/hr PPM @ 3% O2, dry or lb/mmBtu heat input				
		Process Temperature				
	Gaseous Fuel- Fired Equipment	≤ 800° F	> 800 ° F and < 1200° F	≥ 1200 ° F		
	Afterburner, Degassing Unit, Remediation Unit, Thermal Oxidizer, Catalytic Oxidizer or Vapor Incinerator (A)	60 ppm or 0.073 lb/mmBtu	60 ppm or 0.073 lb/mmBtu	60 ppm or 0.073 Ib/mmBtu		
	The emission lim the burner is inci	erate air toxics, V it applies solely v nerating air toxics	OCs, or other vapol when burning 100% s, VOCs, or other va	0% natural gas that rs; or to heat a unit. fuel and not when pors. The unit shall fueled with natural		

District/Agency	Best Available Control Technology (BACT)/Requirements			
	BACT Source: N	ISR Requirements for BACT, page 3-8. (6/2011)		
	Coffee Roaster (A)			
	VOC	Afterburner (0.3 second retention time at 1200 °F)		
	NOx	Natural Gas, with heat recovery on afterburner exhaust to reduce fuel consumption		
	SOx	Natural Gas		
San Diego County APCD	PM10	Natural Gas with cyclone and afterburner (0.3 second retention time at 1200 °F)		
	PM2.5	No standard		
	со	No standard		
	equi	applicant may choose to limit the Potential to Emit (PTE) from the pment to less than 10 pounds per day for each pollutant in lieu of ting the stated BACT requirement.		
	<u>T-BACT</u> There are no T-BACT standards published in the clearinghouse for this category.			
	RULE REQUIREMENTS: None			
	<u>BACT</u> Source: E	3AAQMD BACT Guidelines <u>: 47.1.1 (3/3/1992)</u> , <u>47.3.1 (4/2/2008)</u>		
	Coffee I	Roaster, < 110,00 BTU/hr		
	voc	Afterburner (0.3 second retention time at ≥1200 °F); or catalytic afterburner (≥ 550 °F) – (Technologically Feasible)		
	NOx	 Natural gas firing with combustion modifications – (Technologically feasible) Natural gas firing – (Achieved in Practice) 		
Bay Area AQMD	SOx	Natural Gas		
	PM10	 Natural gas firing with baghouse and afterburner (0.3 second retention time at ≥1400 °F) – (Technologically Feasible) Natural Gas firing with cyclone – (Achieved in Practice) 		
	PM2.5	No standard		
	со	No standard		

District/Agency	Best Available Control Technology (BACT)/Requirements			
	Coffee Roaster, 110,00 BTU/hr to 3.5 MMBtu/hr			
	voc	0.047 lb/ton of beans roasted, afterburner (0.3 second retention time at ≥1400 °F) – (Achieved in Practice)		
	NOx	0.2 lb/MMBtu, natural gas firing – (Achieved in Practice)		
	SOx	Natural gas firing – (Achieved in Practice)		
	PM10	0.01 gr/dscf, Natural Gas with cyclone and afterburner (0.3 second retention time at 1400 °F) – (Achieved in Practice)		
Bay Area AQMD	PM2.5	No standard		
	CO1. 0.1 lb/MMBtu, natural gas firing and use of heat exchangers – (Technologically feasible) 2. 0.4 lb/MMBtu, good combustion practice – (Achieved in Practice)			
	<u>T-BACT</u>			
	Coffee	Roaster, < 110,00 BTU/hr		
	voc	Afterburner (0.3 second retention time at ≥1200 °F); or catalytic afterburner (≥ 550 °F) – (Technologically Feasible)		
	PM10	Natural gas firing with baghouse and afterburner (0.3 second retention time at ≥1400 °F) – (Technologically Feasible)		
	<u>RULE R</u> None	EQUIREMENTS:		
San Joaquin Valley APCD	There ar	SJVUAPCD BACT Guideline e no BACT standards published in the clearinghouse for this category. EQUIREMENTS		

The following control technologies have been identified and are ranked based on stringency:

	SUMMARY OF ACHIEVED IN PRACTICE CONTROL TECHNOLOGIES
Pollutant	Control Technology
VOC	For Coffee Roasters < 110,000 Btu/hr 1. ≥ 90% control efficiency [SMAQMD] 2. Afterburner (≥ 0.3 second retention time at 1200 °F) [SDAPCD] For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. ≥ 90% control efficiency [SMAQMD] 2. 0.047 lb/ton of beans roasted, afterburner (≥ 0.3 second retention time at ≥1400 °F) [BAAQMD] 3. Afterburner (≥ 0.3 second retention time at 1200 °F) [SCAQMD, SDAPCD]
NOx	 For Coffee Roasters < 110,000 Btu/hr 1. Natural gas, with heat recovery on afterburner exhaust to reduce fuel consumption [SDPACD]^(A) 2. Natural gas fuel [SMAQMD, SCAQMD, BAAQMD] For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. For units ≥ 325,000 BTU/hr: 40 ppm NOx at 3% O₂ or 0.049 lb/MMBtu for roaster burners < 500 °F [SMAQMD], 60 ppm NOx at 3% O₂ or 0.073 lb/MMBtu for roaster burners ≥ 500 °F [SMAQMD] 2. For units ≥ 325,000 BTU/hr: 60 ppm NOx at 3% O₂ or 0.073 lb/MMBtu for afterburners, thermal oxidizers, catalytic oxidizers, and vapor incinerators [SCAQMD] 3. Natural gas, with heat recovery on afterburner exhaust to reduce fuel consumption [SDAPCD]^(A) 4. 0.2 lb/MMBtu, natural gas firing [BAAQMD]
SOx	<u>For Coffee Roasters < 110,000 Btu/hr</u> 1. Natural gas fuel [SMAQMD, SCAQMD, SDAPCD, BAAQMD] <u>For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr</u> 1. Natural gas fuel [SMAQMD, SCAQMD, SDAPCD, BAAQMD]
PM10	For Coffee Roasters < 110,000 Btu/hr 1. Natural gas with cyclone and afterburner (≥ 0.3 second retention time at 1200 °F) [SDAPCD] 2. Cyclone and natural gas fuel [SMAQMD] 3. Natural gas fuel [SCAQMD] For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. 0.01 gr/dscf, natural gas with cyclone and afterburner (≥0.3 second retention time at 1400 °F) [BAAQMD] 2. Natural gas with cyclone and afterburner (≥0.3 second retention time at 1400 °F) [BAAQMD] 3. Natural gas with cyclone and afterburner (≥0.3 second retention time at 1400 °F) [SCAQMD] 3. Cyclone and natural gas fuel [SMAQMD]

	SUMMARY OF ACHIEVED IN PRACTICE CONTROL TECHNOLOGIES				
Pollutant	Control Technology				
PM2.5	For Coffee Roasters < 110,000 Btu/hr				
со	For Coffee Roasters < 110,000 Btu/hr				
HAP/VHAP (T-BACT)	 For Coffee Roasters < 110,000 Btu/hr 1. Afterburner (0.3 second retention time at ≥1200 °F); or catalytic afterburner (≥ 550 °F) [BAAQMD] 2. Natural gas firing with baghouse and afterburner (≥0.3 second retention time at ≥1400 °F) [BAAQMD] 				
(T-BACT)	 Afterburner (0.3 second retention time at ≥1200 °F); or catalytic afterburner (a 550 °F) [BAAQMD] Natural gas firing with baghouse and afterburner (≥0.3 second retention time 				

(A) SDAPCD has a BACT trigger level of 10 lbs/day. In order to emit 10 lbs/day of NOx a burner would need to be 4.3 MMBtu/hr, assuming the uncontrolled small boiler NOx emission factor from AP-42, Table 1.4-1 and 24 hrs/day of operation.

BACT for Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr Discussion:

BAAQMD lists emission standards for VOC, NOx, PM10, and CO. However, due to BAAQMD's BACT trigger level of 10 lbs/day only industrial sized facilities trigger these standards. BAAQMD BACT requirements were based on roaster permits for Peet's Coffee and Tea Inc., which have throughputs of 2,200 lbs beans/hr and 3.5 MMBtu/hr burners. Non-industrial roasters have typical throughputs of around 100-600 lbs/hr and burner ratings of 50,000-600,000 btu/hr, based on 12-60 kg capacity roasters. Most permitted coffee roasters in BAAQMD's size category of 110,000 BTU/hr to 3.5 MMBtu/hr have not been source tested to confirm these standards and therefore the emission standards are not considered achieved in practice. However, for the associated control technology are used by almost all roasters and can be considered BACT as these technologies have been achieved in practice.

SDAPCD lists heat recovery on afterburner exhaust to reduce fuel consumption as BACT for NOx. However, due to SDAPCD's BACT trigger level of 10 lbs/day only industrial sized facilities trigger these standards. In order to emit 10 lbs/day of NOx a burner would need to be 4.3 MMBtu/hr and operate 24 hrs/day, assuming the uncontrolled small boiler NOx emission factor from AP-42. Therefore, heat recovery on afterburner exhaust won't be considered achieved in practice for this BACT category of roasters \leq 3.5 MMBtu/hr.

The following control technologies have been identified as the most stringent, achieved in practice control technologies:

BEST CONTROL TECHNOLOGIES ACHIEVED					
Pollutant	Standard	Source			
VOC	For Coffee Roasters < 110,000 Btu/hr 1. ≥ 90% control efficiency, Afterburner (≥0.3 second retention time at 1200 ° F)	SMAQMD, SDAPCD			
	 For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. ≥ 90% control efficiency, lb/ton of beans roasted, afterburner (≥0.3 second retention time at ≥1400 °F) 	SMAQMD, BAAQMD			
	<u>For Coffee Roasters < 110,000 Btu/hr</u> 1. Natural gas fuel	SMAQMD			
NOx	 For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. For units ≥ 325,000 BTU/hr: 40 ppm NOx at 3% O₂ or 0.049 lb/MMBtu for roaster burners < 500°F, 60 ppm NOx at 3% O₂ or 0.073 lb/MMBtu for roaster burners ≥ 500 °F 2. For units ≥ 325,000 BTU/hr: 60 ppm NOx at 3% O₂ or 0.073 lb/MMBtu for afterburners, thermal oxidizers, octobric oxidizers, and waper incidentation 	SMAQMD, SCAQMD			
	catalytic oxidizers, and vapor incinerators				
SOx	For Coffee Roasters < 110,000 Btu/hr 1. Natural gas fuel	SMAQMD, SCAQMD, SDAPCD, BAAQMD			
	For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 2. Natural gas fuel	SMAQMD, SCAQMD, SDAPCD, BAAQMD			
PM10	 For Coffee Roasters < 110,000 Btu/hr 1. Natural gas with cyclone and afterburner (≥0.3 second retention time at 1200 °F) 	SDAPCD			
PM10	 For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. Natural Gas with cyclone and afterburner (≥0.3 second retention time at 1400 °F) 	BAAQMD			
	For Coffee Roasters < 110,000 Btu/hr 1. Cyclone and natural gas fuel	SMAQMD			
PM2.5	For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. Cyclone and natural gas fuel	SMAQMD			
	For Coffee Roasters < 110,000 Btu/hr 1. Natural gas fuel and good combustion practices	SMAQMD			
со	For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. Natural gas fuel, and good combustion practices.	SMAQMD, BAAQMD			

BEST CONTROL TECHNOLOGIES ACHIEVED				
Pollutant Standard Source				
HAP/VHAP (T-BACT)	 For Coffee Roasters < 110,000 Btu/hr 1. Afterburner (≥0.3 second retention time at ≥1200 °F); or catalytic afterburner (≥ 550 °F) 2. Natural gas firing with baghouse and afterburner (≥0.3 second retention time at ≥1400 °F) 	BAAQMD		

B. TECHNOLOGICALLY FEASIBLE AND COST EFFECTIVE (Rule 202, §205.1.b.):

Technologically Feasible Alternatives:

Any alternative basic equipment, fuel, process, emission control device or technique, singly or in combination, determined to be technologically feasible by the Air Pollution Control Officer.

The table below shows the technologically feasible alternatives identified as capable of reducing emissions beyond the levels determined to be "Achieved in Practice" as per Rule 202, §205.1.a.

Pollutant	Technologically Feasible Alternatives
VOC	No other technologically feasible option identified (A)
NOx	No other technologically feasible option identified
SOx	No other technologically feasible option identified
PM10	<u>For Coffee Roasters < 110,000 Btu/hr</u> (A) Baghouse and afterburner (≥0.3 sec retention time at ≥1400°F)
PM2.5	No other technologically feasible option identified
со	For Coffee Roasters 110,000 Btu/hr to 3.5 MMBtu/hr 1. 0.1 lb/MMBtu, natural gas firing with use of heat exchangers [BAAQMD]

(A) BAAQMD lists an afterburner with a 0.3 retention time as technologically feasible for both VOC and PM10 for coffee roasters less than 110,000 Btu/hr. However, an afterburner with a 0.3 retention time for roasters less than 110,000 Btu/hr is considered achieved in practice by SMAQMD and SDAPCD BACT determinations.

Cost Effective Determination:

After identifying the technologically feasible control options, a cost analysis is performed to take into consideration economic impacts for all technologically feasible controls identified.

Maximum Cost per Ton of Air Pollutants Controlled

1. A control technology is considered to be cost-effective if the cost of controlling one ton of that air pollutant is less than the limits specified below (except coating

operations):

<u>Pollutant</u>	Maximum Cost (\$/ton)
ROG	17,500
NO _X	24,500
PM10	11,400
SO _X	18,300
CO	TBD if BACT triggered

Cost Effectiveness Analysis Summary

The cost analysis was processed in accordance with the EPA OAQPS Air Pollution Control Cost Manual (Sixth Edition). The sales tax rate was based on the District's standard rate of 8.5% as approved on 10/17/16. The electricity (13.8 cents/kWh) rates were based on a commercial application as approved by the District on 10/17/16. The life of the equipment was based on the EPA cost manual recommendation. The interest rate was based on the previous 6-month average interest rate on United States Treasury Securities (based on the life of the equipment) and addition of two percentage points and rounding up to the next higher integer rate. The labor (Occupation Code 51-3091: Food and Tobacco Roasting, Baking, and Drying Machine Operators and Tenders) and maintenance (Occupation Code 49-9099: Installation, maintenance, and repair workers, all other) rates were based on data from the Bureau of Labor Statistics.

Baghouse:

Equipment Life = 20 years Total Capital Investment = \$11,680.84 Direct Annual Cost = \$8,106.54 per year Indirect Annual Cost = \$5,873.19 per year Total Annual Cost = \$13,979.74 per year PM10 Removed = 0.31 tons per year

Cost of PM10 Removal = \$45,060.32 per ton reduced

A detailed calculation of the cost effectiveness for PM10 removal with a baghouse is shown in Attachment B. As shown above, the cost of venting the emissions to a baghouse is not cost effective.

CO BACT

BACT for CO is not triggered for this type of source and would only be triggered for extremely large process rates. Therefore, a cost effective analysis for BAAQMD's CO BACT for roasters between \geq 110,000 Btu/hr to 3.5 MMBtu/hr won't be evaluated for this BACT determination. BAAQMD identified 0.1 lb/MMBtu and natural gas firing with use of heat exchangers as technologically feasible.

The CO BACT trigger for SMAQMD is emissions greater than 550 lb/day. At 3.5 MMBtu/hr and a CO emission factor of 295.5 lb/MMcf (400 ppm CO), the worst case natural gas combustion emissions for 24 hours of operation would be 24.8 lbs CO per day. The CO emissions of a continuous roaster per AP-42 is 1.5 lb/ton coffee roasted. If a roaster operated for 24 hours, in order to trigger BACT for CO a roaster would need to process at least 350

BACT Determination Coffee Roasters ≤ 3.5 MMbtu/hr Page 12 of 13

tons of coffee beans per day. Therefore, it is highly unlikely that any coffee roasting source of this size would trigger BACT for CO. If BACT for CO is ever triggered for a coffee roaster, a new BACT will be made at that time.

C. SELECTION OF BACT:

Based on the cost effectiveness determinations, BACT for NOx will remain at what is currently achieved in practice and BACT for PM2.5 will be set to be the same as for PM10 (use of natural gas).

	BACT # 141 FOR COFFEE ROASTERS < 110,000 BTU/HR				
Pollutant Standard Source					
VOC	≥ 90% control efficiency, Afterburner (≥0.3 second retention time at 1200 ° F) or equivalent technology	SMAQMD SDAPCD			
NOx	Natural gas fuel	SCAQMD			
SOx	Natural gas fuel	SMAQMD, SCAQMD, SDAPCD, BAAQMD			
PM10	Natural gas fuel with cyclone and afterburner (0.3 second retention time at 1200 ° F) or equivalent technology	SDAPCD			
PM2.5	Cyclone and natural gas fuel	SMAQMD			
СО	Natural gas fuel and good combustion practices	SMAQMD			

BAC	BACT # 184 FOR COFFEE ROASTERS 110,000 BTU/HR to 3.5 MMBTU/HR				
Pollutant	Standard	Source			
VOC	≥ 90% control efficiency, afterburner (≥0.3 second retention time at ≥1400 °F) or equivalent technology	SMAQMD, BAAQMD			
NOx	 For units ≥ 325,000 BTU/hr: 40 ppm NOx at 3% O₂ or 0.049 lb/MMBtu for roaster burners < 500 °F, 60 ppm NOx at 3% O₂ or 0.073 lb/MMBtu for roaster burners ≥ 500 °F For units ≥ 325,000 BTU/hr: 60 ppm NOx at 3% O₂ or 0.073 lb/MMBtu for afterburners, thermal oxidizers, catalytic oxidizers, and vapor incinerators 	SMAQMD, SCAQMD			
SOx	Natural gas fuel	SMAQMD, SCAQMD, SDAPCD, BAAQMD			
PM10	Natural gas with cyclone and afterburner (≥0.3 second retention time at 1400 ° F) or equivalent technology	BAAQMD			
PM2.5	Cyclone and natural gas fuel	SMAQMD			
со	Natural gas fuel and good combustion practices	SMAQMD, BAAQMD			

BACT Determination Coffee Roasters ≤ 3.5 MMbtu/hr Page 13 of 13

D. SELECTION OF T-BACT:

The toxics at issue with this technology are VOCs. The control of VOCs through meeting the BACT standard will also control toxics found in the VOCs. Therefore, the BACT VOC controls are also the T-BACT controls.

APPROVED BY: Bri Fluch DATE: 9-4-19

Attachment A

BACT Determinations form SMAQMD, SCAQMD, SDAPCD, & BAAQMD

REPLACED

BACT Size	Minor Source	BACT	COFFEE ROASTER V	W/ AFTERBURNE
BACT Det	ermination Numb	er: 100	BACT Determination Date:	1/30/2015
		Equipment	Information	
Permit Nu	mber: N/A	Generic BACT Determination	n	
Equipmen	t Description:	COFFEE ROASTER W	AFTERBURNER	
Unit Size/	Rating/Capacity:	Minor Source BACT		
Equipmen	t Location:			
		BACT Determina	tion Information	
	1			
ROCs	Standard:	≥90% control efficiency	ter burner and ≥0.3 second retention time at 120	WE to be reached
	Technology Description:	in the final 5 minutes of the roas		o F, to be reached
	Basis:	Achieved in Practice		
NOx	Standard:			
	Technology	Natural Gas Fuel		
	Description:			
	Basis:	Achieved in Practice		
SOx	Standard:			
	Technology	Natural Gas Fuel		
	Description:			
	Basis:	Achieved in Practice		
PM10	Standard:	Cyclone and Natural Gas Fuel		
	Technology	Cyclone and Natural Gas Fuel		
	Description: Basis:	Achieved in Practice		
D140 5	Standard:			
PM2.5	Technology	Cyclone and Natural Gas Fuel		
	Description:			
	Basis:	Achieved in Practice		
со	Standard:			
	Technology	Natural gas fuel and good comb	ustion practices	
	Description:			
	Basis:	Achieved in Practice		
LEAD	Standard:			
	Technology			
	Description: Basis:			
Comment	s: This is a generic B/ California and/or ot		T determinations made, and published, by other a	air agencies in

SCAQMD

10-20-2000 Rev. 0 2-1-2019 Rev. 1

Equipment or Process: Coffee Roasting

		Crit	eria Pollutants			
Subcategory/ Rating/Size	VOC	NOx	SOx	CO	PM 10	Inorganic
Roaster, < 110,000 BTU/Hr		Compliance with Rule 1147 (2-1-2019)	Natural Gas (1988)		Natural Gas (1988)	
Roaster, ≥ 110,000 BTU/Hr	Afterburner (0.3 Sec Retention Time at 1200 °F) (1990)	Compliance with Rule 1147 (2-1-2019)	Natural Gas (1990)		Natural Gas with Cyclone and Afterburner (≥ 0.3 Second Retention Time at ≥ 1200 °F) (1990)	
Handling Equipment, < 1,590 Lbs/Hr All ¹						
Handling Equipment, ≥ 1,590 Lbs/Hr All					Cyclone (1990)	

1) At the date of the last revision for this category, there was no Achieved In Practice BACT Determination for this subcategory. Technologically Feasible options listed in historic SCAQMD BACT Guidelines for this subcategory require cost effective analyses before they can be listed in these current Guidelines.

SDAPCD

COFFEE ROASTERS Fee Schedule 50A

Review the BACT Control Option listed below. The applicant must propose the Control Option listed or perform a Top-down BACT Analysis as described in Section 4 to justify the selection of another Control Option. The applicant will be required to provide documentation that the Control Option selected meets the requirements listed in the table.

	VOC	NOx	SOx	PM
BACT Emission Rate Limit	Not Determined	Not Determined	Not Determined	Not Determined
BACT Control Option	Afterburner (0.3 sec retention time at 1200 degrees F	Natural gas with heat recovery on afterburner exhaust to reduce fuel consumption	Natural gas	Natural gas with cyclone and afterburner (0.3 sec retention time at 1200 degrees F
		(A/P)	(A/P)	(A/P)

The applicant may choose to limit the Potential to Emit (PTE) from the equipment to less than 10 pounds per day for each pollutant in lieu of meeting the stated BACT requirement.

Source Category

		Revision:	2
Source:	Coffee Roasting	Document #:	47.1.1
Class:	< 110,000 Btu/hr	Date:	03/03/92

Determination

POLLUTANT	BACT 1. Technologically Feasible/ Cost Effective 2. Achieved in Practice	TYPICAL TECHNOLOGY
POC	1. Afterburner (≥ 0.3 sec. retention time at $\geq 1200^{\circ}F$); or catalytic afterburner ($\geq 550^{\circ}F$) ^{a,b,T} 2. n/d	 BAAQMD Approved Design and Operation^b n/d
NOx	 Natural gas firing with combustion modifications^{a,b} Natural gas firing^{a,b} 	 BAAQMD Approved Design and Operation^b Fuel Selection^b
so ₂	1. Natural gas firing ^b 2. Natural gas firing ^b	 Fuel Selection^b Fuel Selection^b
со	1. n/d 2. n/s	1. n/d 2. Good Combustion Practice ^b
PM ₁₀	 Natural gas firing with baghouse and afterburner (≥ 0.3 sec retention time at ≥1400°F)^{a,b,T} Natural gas firing with cyclone^b 	 BAAQMD Approved Design and Operation^b BAAQMD Approved Design and Operation^b
NPOC	1. n/a 2. n/a	1. n/a 2. n/a

References

а.	SCAQMD Guideline
b.	BAAQMD
Т.	TBACT

BAY AREA AIR QUALITY MANAGEMENT DISTRICT Best Available Control Technology (BACT) Guideline

Source Category

Source:	Coffee Roasting	Revision:	1
	cojjec reasing	Document #:	47.3.1
Class:	110,000 BTU/hr to 3.5 MM BTU/hr	Date:	4/2/08

Determination

POLLUTANT	BACT 1. Technologically Feasible/ Cost Effective 2. Achieved in Practice	TYPICAL TECHNOLOGY
POC	1. n/d 2. 0.047 lb/ton of beans roasted	1. n/d 2. Afterburner (≥ 0.3 sec. retention time at $\geq 1400^{\circ}F$) ^a
NOx	1. n/d 2. 0.2 lb/MMBTU ⁴	1. n/d 2. Natural Gas Firing ^a
SO ₂	1. Natural gas firing ^a 2. Natural gas firing ^a	 Fuel Selection^a Fuel Selection^a
со	1. 0.1 lb/MMBTU 2. 0.4 lb/MMBTU	 Natural Gas Firing & Use of Heat Exchangers^a Good combustion practice^a
PM10	1. n/d 2. 0.01 gr/dscf ^a	 n/d Natural gas firing with cyclone and afterburner (≥ 0.3 sec retention time at ≥1400°F)^a
NPOC	1. n/a 2. n/a	1. n/a 2. n/a

References

a. BAAQMD Application # 13807 & 15187

Attachment B

Cost Effectiveness Determination for Baghouse

COST EFFECTIVENESS ANALYSIS FOR BAGHOUSE

This cost effectiveness analysis was performed using EPA's OAQPS Control Cost Manual

EPA publication No. 452/B-02-001, Chapte	^r 1, Baghouses and Filters (12/98)

FACILITY NAME:	Temple	
LOCATION:	2827 S St., Sacrame	nto
PERMIT NO.:	25127	
EQUIPMENT		
DESCRIPTION:	Coffee Roaster	
PM10 Baghouse		
Cost Effective		
Requirements		
Coffee beans		
processed	546.5	lb/hr
PM10 Emission		
Factor	1.114	lb/ton
PM Emission Rate	0.304	lb/hr
Hours per day	8	
Days per week	5	
Weeks per year	52	
PM emission from		
coffee roasting		
operation	0.31657652	tons/year
Baghouse Control		
Efficiency	98%	
Controlled PM		
Emissions	0.31	tons/year
CRF (5% interest		
and 20 year life)	0.080242587	
Particulate Matter C	ontrol (Bag House)	
Cost Analysis		
Gas to cloth ratio		
for shaker or		
reverse air bag		
house	2.8	Table 1.1
A	15	Table 1.4
В	1	Table 1.4
L	0.1	
D	10	
V	11.11956286	equation 1.11
acfm of system	900	acfm
Bag Size	80.93843355	ft^2
0		1

BACT Determination Coffee Roasters ≤ 3.5 MMbtu/hr Attachment B – Cost Effectiveness Analysis Page 2 of 3

Cost of Pag house		
Cost of Bag house		
common housing	¢ 2,000 70	
design	\$ 2,886.76	
Cost of insulation	\$ 1,221.49	
Cost of bag (Pulse		
jet, BBR - fiberglass,		
Table 1.8), bottom	4	
bag removal	\$ 136.79	
Bag house cages	\$ 6.03	
cage cost	\$ 12.23	\$/cage
Total cage costs	\$ 73.76	
Equipment Costs		
(A)	\$ 4,318.80	
	4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	
Instrumentation	\$ 431.88	0.10*A
California Sales		
taxes	\$ 367.10	0.085*A
Freight	\$ 215.94	0.05*A
Purchase		
Equipment Cost		
(PEC)	\$ 5,333.72	
		
Direct Installation		
Costs		
Foundation &	A 040 05	
Supports	\$ 213.35	0.04*PEC
Handling & erection	\$ 2,666.86	0.50*PEC
Electrical	\$ 426.70	0.08*PEC
Piping	\$ 53.34	0.01*PEC
Insulation for		
ductwork	¢ 272.26	
Painting	\$ 373.36	0.07*PEC
	\$ 373.36 \$ 213.35	0.07*PEC 0.04*PEC
Total direct		
Total direct installation costs		
installation costs	\$ 213.35	
installation costs Indirect Costs	\$ 213.35	
installation costs Indirect Costs (installation)	\$ 213.35 \$ 3,946.95	0.04*PEC
installation costs Indirect Costs (installation) Engineering	\$ 213.35	
installation costs Indirect Costs (installation) Engineering Construction and	\$ 213.35 \$ 3,946.95 \$ 533.37	0.04*PEC 0.10*PEC
installation costs Indirect Costs (installation) Engineering Construction and field expense	\$ 213.35 \$ 3,946.95 \$ 533.37 \$ 1,066.74	0.04*PEC 0.10*PEC 0.20*PEC
installation costs Indirect Costs (installation) Engineering Construction and	\$ 213.35 \$ 3,946.95 \$ 533.37 \$ 1,066.74 \$ 533.37	0.04*PEC 0.10*PEC 0.20*PEC 0.10*PEC
installation costs Indirect Costs (installation) Engineering Construction and field expense Contractor fees Startup-up	\$ 213.35 \$ 3,946.95 \$ 533.37 \$ 1,066.74 \$ 533.37 \$ 533.37 \$ 533.37	0.04*PEC 0.10*PEC 0.20*PEC 0.10*PEC 0.01*PEC
installation costs Indirect Costs (installation) Engineering Construction and field expense Contractor fees	\$ 213.35 \$ 3,946.95 \$ 533.37 \$ 1,066.74 \$ 533.37 \$ 53.34 \$ 53.34	0.04*PEC 0.10*PEC 0.20*PEC 0.10*PEC
installation costs Indirect Costs (installation) Engineering Construction and field expense Contractor fees Startup-up Performance test Contingencies	\$ 213.35 \$ 3,946.95 \$ 533.37 \$ 1,066.74 \$ 533.37 \$ 533.37 \$ 533.37	0.04*PEC 0.10*PEC 0.20*PEC 0.10*PEC 0.01*PEC
installation costs Indirect Costs (installation) Engineering Construction and field expense Contractor fees Startup-up Performance test	\$ 213.35 \$ 3,946.95 \$ 533.37 \$ 1,066.74 \$ 533.37 \$ 53.34 \$ 53.34	0.04*PEC 0.10*PEC 0.20*PEC 0.10*PEC 0.01*PEC 0.01*PEC

BACT Determination Coffee Roasters ≤ 3.5 MMbtu/hr Attachment B – Cost Effectiveness Analysis Page 3 of 3

Total Capital		
Investment (TCI)		
(PEC+DC+IC)	\$11,680.84	
Direct Annual Costs		
Operating Labor	\$2,011.10	(.5 hr/shift) (1 shift/8 hrs)(2080 hrs/yr)*\$15.47
Supervisor	\$301.67	15% of operating Labor
Maintenance Labor	\$2,567.50	(.5 hr/shift) (1 shift/8 hrs)(2080 hrs/yr)*\$19.75
Material	\$2,567.50	100% of maintenance labor
Bag replacement		
labor	\$0.19	\$/ft2 of bag area
CRF for bags (5%		
interest and 2 year		
life)	0.54	
Replacement Parts,		
Bags	\$123.45	equation 1.13
		(0.000181)(900 acfm)(10 in H2O)(2080 hr/yr)(\$0.138
Electricity	\$467.59	kW/h)
		(2scfm/1000acfm)*900cfm*(\$0.25/1000scf)*(60min/hr)*
Compressed Air	\$56.16	(2080hr/year)
Waste Disposal	\$10.86	\$35/ton
Total Annual DC	\$8,106.54	
Indirect Annual		
Costs		
Overhead	\$4,468.66	60% of total labor and material
Admin charges	\$233.62	2% of TCI
Property Tax	\$116.81	1% of TCI
Insurance	\$116.81	1% of TCI
Capital Recovery	\$937.30	
Total Annual IC	\$5,873.19	
Total Annual Costs		
(DAC + DIC)	\$13,979.74	
TAC/tons controlled	\$45,060.32	